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New Pyrolysis Mechanisms for Dust Explosion Simulation

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Numerical simulation of dust explosions can be used for intensive, multi-parameter sensitivity studies, reducing the number of experimental tests required. Nevertheless, to develop such approaches, it is imperative to collect reliable input data beforehand. Preliminary tests show that particular attention needs to be paid to developing new flash pyrolysis mechanisms. Indeed, simple devolatilization reactions (polymer into monomer conversion) are not suitable, and the chemical species to be considered are far more numerous than in the case of lighter chemical compounds or shorter chains. On the other hand, the mechanical properties of synthetic polymers seem to limit their fragmentation in the 20L sphere, which could simplify the simulation approach by neglecting particle sizes modification.

* 1. Introduction

The experimental determination of explosion severity parameters is based on international standards, which generally set arbitrarily the test conditions. However, these conditions are not always those encountered in industrial processes (e.g. high ignition energy and turbulence, particle size distribution (PSD) changes due to powder dispersion in the explosion vessels…) and although the test results are generally conservative, the consequences of this deviation from reality need to be assessed. It should be noted that the term “reality” is certainly inappropriate, as it covers a wide variety of situations that can arise on the same industrial site. In this case, it is more appropriate to describe a range of realistic conditions considered during major risk assessment.

Then, the process safety expert has several options: a) From among all probable situations, to determine the most conservative conditions and carry out tests based on these parameters only; This is often the case when the powder is sieved, dried and tested at high ignition energies; b) To carry out an extensive sensitivity study to determine the influence of variations in operating parameters, which requires a very large number of experiments, and is therefore time-consuming and costly; c) To acquire in-depth knowledge of the phenomenon and use numerical simulation to test all the effects of such variations, but this solution cannot be implemented on its own without a preliminary experimental validation.

In this work, the latter approach was favoured and both Computational Fluid Dynamics (CFD) simulation and experimental approach were combined to represent the explosion of organic powders. Several articles were already published on this subject (Islas et al., 2023; Portarapillo et al., 2021; Zhang et al., 2024) but most of the studies combining CFD and dust explosion only consider the powder dispersion stage, without simulating the reaction stages of pyrolysis, oxidation/combustion, and flame propagation within the 20L sphere (Pico et al., 2020). In parallel, numerous studies were focused on determining the reaction mechanisms describing the pyrolysis and/or combustion phases of organic compounds. However, it is rare to obtain this information under the specific conditions of a dust explosion. Indeed, experimental characterizations based on objects of different sizes (millimetre range powders, polymer slabs...), low temperature ramps or oxidation/pyrolysis conditions different from those observed during an explosion, although useful, cannot be directly used within the framework of a numerical simulation.

The aim of this work is to propose lumped mechanisms for the pyrolysis of synthetic or natural organic powders, so that they can be incorporated into CFD simulations of a dust explosion. Indeed, both identifying pyrolysis gases and proposing pyrolysis mechanism is a key-point in modelling a dust explosion (Jiang et al, 2024). Such development will provide insights, either into predicting the severity of a dust explosion within a 20L vessel, based on the powder properties, or into predicting the potential consequences of a dust explosion in a complex industrial configuration, based on empirical data obtained using a 20L sphere. Knowledge of pyrolysis mechanisms will also be useful for thermal conversion processes of polymers (e.g. waste plastics) and will improve the adjustment of safety parameters for powders at high temperatures. This article presents a state of the art, the methodology and preliminary work carried out on two powders (polyethylene and polystyrene).

* 1. State of the art

This section will be devoted to a brief bibliographical survey of the state of the art in relation to the CFD of dust explosions, mainly in 20L spheres. The second section will highlight the importance of the reaction mechanisms considered for the simulation.

* + 1. CFD simulation of dust dispersion at laboratory scale

The dynamics of dust dispersion in the 20-L test sphere has already been thoroughly studied (Table 1). The influence of various parameters including nozzle geometry, ignition delay time and particle size distribution have been considered. The first challenge of a dust dispersion in the 20L sphere is to ensure a uniform dissemination of the dust inside the vessel. A uniform distribution theoretically guarantees the consistency and reproducibility of the test, but sedimentation and certain physical properties such as a wide PSD, shapes or density may cause heterogeneities (Li et al., 2020; Ray et al., 2020). The second challenge is the control of the dust cloud turbulence, which has a significant effect on the explosion severity and flame propagation (Islas et al., 2022). To improve dust dispersion, different types of nozzles can be designed (Pico et al., 2020). The third challenge is to take account of the ignition phase and its instability, which is, by their very nature, a transient phenomenon (Portarapillo et al., 2021). Finally, correctly describing the reaction kinetics of the powder (heating, pyrolysis/devolatilization, gas oxidation) is a major challenge (Bind et al., 2012; Islas et al., 2022; Pico et al., 2020; Wang et al., 2020) (Table 1).

Table 1: Summary of relevant CFD studies dealing with dust explosion in a 20L vessel

|  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- |
| Reference | Powders | CFD software | Scenario | Turbulence model | Description |
| Bind et al.,  2012 | Aluminium and starch | Ansys  Fluent | **Developing multi-scale (particle and cloud) reaction engineering model** | standard k−ϵ model | Combustion at the particle scale for Al and group combustion for starch. Single reaction |
| Li et al.,  2020 | Cornstarch | Ansys  Fluent | Effects of oxygen, fuel concentration and PSD | standard k−ϵ model | Highlight the influence of flame-turbulence interactions |
| Islas et al.,  2022 | Biomass (Pellets Asturias and Cupressus Funebris) | OpenFOAM | Biomass dusts explosion is mainly governed by the characteristics of the cold-flow | Eulerian-Lagrange with 2-way coupling | Moisture  evaporation, devolatilization, and char oxidation are considered for the reactions |
| Pico et al.,  2020 | Wheat  starch | Ansys  Fluent | Three different nozzles. Pyrolysis step considered and  solid/gas hybrid mixtures | CFD-DPM (Discrete Phase Model) with a Eulerian-Lagrange | Powder dispersion and the pyrolysis/gas oxidation reactions  Pyrolysis gases from modified G-G furnace |
| Portarapillo et al., 2021 | Various classes of dusts (A to D) | Ansys  Fluent | Comparison between 20L and 1m3 explosion vessels.  Influence of chemical igniters | URANS  standard k−ϵ model | Flame propagation and heat transfers generated by pyrotechnic ignitors and their impact on different kinds of dusts |
| Ray et al.,  2020 | Coal dust | Ansys  fluent | Dispersion of coal  dust in a **20-L vessel** | standard k−ϵ model | Dust dispersion in an 20L explosion chamber |
| Wang et al.,  2020 | Corn starch | Ansys  Fluent | Three steps-  process including devolatilization.  3 ignition modes | standard k−ϵ model | 2 pyrolysis reactions, Single gas combustion reaction, and 2 char combustion reactions |

CFD corrections can be proposed to take the discrepancies between ‘ideal dispersion’ and reality into account as such variations can lead to a substantially under-prediction of explosion severity for larger particles (Islas et al., 2022). The influence of particle concentration on biomass dust explosion characteristics found significant changes in explosion properties. Low concentration may lead to incomplete burning, while high concentration can increase the flame propagation, and also increases the risk of secondary explosion.

However, excessive turbulence can extinguish the flame prematurely or spread unevenly because turbulence plays a dual role: enhancing both dispersion and combustion efficiency. Pico et al., 2020 explored hybrid dust-gas systems, such as wheat starch and pyrolysis gases. Their results show that interactions between gas-phase reactions and dust combustion can enhance turbulence and explosion intensity. This underscores the importance of considering mixed-phase reactions in explosion modeling.

* + 1. Importance of pyrolysis mechanisms

Several authors have attempted to describe the reaction kinetics of powders in a dust explosion by simplifying the various reactions into lumped mechanisms as shown in Table 2. Some authors have considered single steps, either a devolatilization step (Quek et al, 2022) or a reaction step (Bind et al, 2012). Depending on the physico-chemical properties of the powders, or for convenience, it is sometimes appropriate to consider heterogeneous and homogeneous reactions simultaneously (Li et al., 2020). But the stages of an organic dust explosion are invariably the same: heating of the particles, pyrolysis and oxidation of the gases, and neglecting one of these phases can only be justified by determining the rate-limiting step. Therefore, other authors have proposed to develop mechanisms that clearly separate the pyrolysis and oxidation phases (Pico et al., 2020). Islas et al. (2022) have proposed a comprehensive model that also takes into account the particle drying phase. Finally, it should be pointed out that Table 2 is not intended to be exhaustive, and that other reaction models have been proposed, notably for carbonaceous powders (Khan et al., 2024).

Table 2: Summary of some CFD studies of dust explosion – focus on the reaction mechanisms

|  |  |  |  |
| --- | --- | --- | --- |
| Reference | Pyrolysis gases | Reaction mechanisms | Model validation |
| Bind et al.  2012 | No | Single combustion reaction for starch: CO2 and H2O generation  Beckstead combustion time correlation for Al: single reaction | Pressure-time curves from simulation and experimental results, with flame propagation speeds and temperature profiles. |
| Islas A.  2022 | CO, CO₂, CH₄, and H₂ | Moisture evaporation rate  Devolatlization (SFOM & BioCPD)  Surface reaction (C + O2) | Pressure-time curves from simulation and experimental results, peak pressures |
| Li et al.,  2020 | Volatiles  CO, H₂, CH₄, C2H₄ | Combination of heterogeneous combustion of C (with O2 or H2O) and oxidation of the so-called volatiles | Pressure-time curves, flame characteristics (flame length, spatial velocity) |
| Pico P.  2020 | Pyrolysis gases  (CO, CH4, C2H4 and H2) + tar (C2H4O) | 4 steps pyrolysis, gas oxidation, turbulence-chemistry interactions, and a combination of gas- and solid-phase reactions | Validated with experimental data from pressure-time curves and pyrolysis gases determined from micro-gas chromatography |
| Quek et al.,  2022 | C2H4 | Devolatilization of PE into C2H4 and “heterogeneous reaction of LDPE and C2H4” | Pressure-time curves. Literature data from LDPE/C2H4 explosion |

3. Materials and methods

CFD simulations require both input data, describing for instance the initial particle size distribution of the powders and the pyrolysis and oxidation mechanisms, and validation data sets of explosion severity parameters.

* + 1. Powders

Two kinds of powders were used in this study: natural polymers, such as cellulose, lignin or starch and synthetic polymers, as polyethylene, polypropylene, poly(methyl methacrylate), polylactic acid or polystyrene. Powders were selected for their composition (low additive content) and their fine PSD. Indeed, grinding of polymers, especially those exhibiting good plastic or elastic properties, was avoided as heat modifies their surface properties. The particle size distribution was determined both ex-situ and in-situ, i.e. in the 20L sphere during the powder injection phase. As stated in introduction, this article focuses on polystyrene (PS) and polyethylene (PE 35-50 µm from VWR).

* + 1. Pyrolysis gases and mechanisms determination

In order to reproduce as much as possible the conditions of a dust explosion, the pyrolysis mechanisms must be determined for a powder dispersed in air, undergoing a rapid rise in temperature from ambient temperature to pyrolysis temperature (generally, greater than 350-450°C at the surface of the polymer). Residence times should be short, on the order of a few tens of milliseconds to 200 ms, and the oven temperature should reach 500 to 1000°C. Therefore, a modified Godbert-Greenwald furnace was used to analyze the gaseous compounds generated by the flash pyrolysis of the polymers. The furnace was made air-proof inserting an inner Inconel cylinder. The entire set-up was flushed with argon during 15 to 30 minutes before injecting the powder (0.2 to 0.5 g) with the same gas at pressures ranging from 0.1 to 0.5 barg. The pyrolysis gases collected in a Tedlar bag were analyzed by gas chromatography GC (SRA 3000 µGC with a TCD detector - 3 ways). Permanent gases (e.g. H2, CO, CO2, CH4, C2H2, C2H4, C2H6) were measured, as well and aromatic compounds (benzene, xylene…). Additional calibrations may be necessary to identify unknown compounds.

* + 1. 20L spheres: dust cloud properties and explosion severity

Explosion severity, characterized by the maximum explosion pressure pm and maximum rate of pressure rise dp/dtm, was determined in a standard 20L sphere according to EN 14034 series. The ignition energy and ignition delay time were set at 10 kJ and 60 ms, respectively. The dust dispersion is ensured by using a rebound nozzle.

The PSD of the dust cloud was determined in-situ at the centre of the 20L sphere as a function of time. A replica of the standard 20L sphere, equipped with 4 windows and with the same dust dispersion system (dust canister, inlet valve, rebound nozzle), was used jointly with a laser diffraction sensor (Helos - Sympatec). The acquisition frequency was set at 5 ms and the analysis range extended from 0.5 to 175 µm.

Particle Image Velocimetry (PIV) will also be applied to the same vessel to characterize the initial turbulence of the dust cloud. Root-mean-square (RMS) velocity of around 5 m.s-1 are expected at ignition time (Murillo, 2016).

* + 1. Numerical simulation

CFD simulation of dust dispersion and flame propagation in a 20 L sphere was carried out using a Euler–Lagrange method (Ansys Fluent). Spatial discretization uses the finite volume method (polyhedral and prismatic cells). Various fluid properties, including the pressure field, velocity field, turbulence intensity, and degree of particle dispersion (spatial repartition of the dust cloud), were obtained and compared with the experimental results. The combustion reaction of the powders was considered via two main steps: the generation of pyrolysis gases followed by their oxidation.

For simulation purposes, the explosion vessel was divided into three parts: a 20L sphere, a standard nozzle, and a dust container, all treated as internal walls without any inlet or outlet conditions in this geometry. All internal walls are defined with a no-slip condition for the gas flow. The calculation parameters of the CFD simulation are defined as a two-phase flow and analyzed with an implicit unsteady formulation. The two-way coupling treats the particles carried by the fluid in a Eulerian-Lagrangian approach, so that the equations of the dust phase are set to a group of particles (or parcel) sharing the same properties.

Spatiotemporal discretization uses a hybrid scheme that blends pure central differencing with the second-order upwind scheme, guided by the Detached Eddy Simulation model for turbulence evolution. Mesh generation was done with a maximum growth rate of 1.3. The edge size ranges from 0.5 mm (near the nozzle) to 16 mm, with a total number of cells kept between 1 and 2,000,000 to ensure manageable computation time. Calculations were done using a server equipped with an Intel Xeon W7-3545 processor at 2.71 GHz and 512 GB of RAM.

Pyrolysis reactions were taken from a simplified global mechanism based on experimental data collected with the Godbert-Greenwald furnace. The oxidation step of the pyrolysis gases was modelled by the CHEMKIN interface. The methodology couples CFD with detailed chemical kinetics. The fluid flow and dispersion dynamics within the 20 L sphere are simulated, and Fluent solves the Navier-Stokes equations, tracking reactant dispersion and evolving concentration fields. Integration of a new pyrolysis mechanism is made via CHEMKIN files, incorporating species transport, reaction rates, and thermal feedback. This coupling predicts species concentrations, temperature profiles, and reaction rates over time. Parametric studies will assess the effects of varying initial conditions, such as fuel concentration and PSD.

Initial simulations confirm the non-uniform nature of the powder dispersion in the sphere and highlight the impact of the powder (PSD, concentration) on turbulence before and after ignition (Murillo, 2016; Pico et al., 2020).

One of the main limitations of using CFD is its computational cost. In this study, simplifications will be necessary in order to limit the computation time, such as the assumption of a constant PSD (section 3.1), the use of lumped kinetic models or the fact of neglecting the deformation of the nozzle during injection. The effects of flame quenching at the wall (particularly radical terminations) are also delicate points to consider.

* 1. Results

Preliminary tests were performed on polystyrene and polyethylene dusts.

* + 1. In-situ particle size distribution

Knowledge of the PSD of the dust cloud before its ignition is essential as it can be strongly different from that determined by dry or wet ex-situ particle size measurement. Figure 1 shows that the PSD of polystyrene significantly changes during its injection in the sphere. Given the difficulty of grinding this type of material, it is unlikely that powder fragmentation can be envisaged. However, the detachment of fine particles attached by electrostatic forces to the primary powders or a change in the powder shape must be considered. Polyethylene being finer, with a primary PSD ranging from 35 to 50 µm, the time-evolution of its PSD is less noticeable. However, the presence of finer particles (< 20 µm) should be highlighted.

Une image contenant texte, ligne, Tracé, diagramme

Description générée automatiquement

*Figure 1: Time-evolution of the PSD of polystyrene and polyethylene powders in the 20L sphere*

* + 1. Pyrolysis gases of polymers

Table 3 summarizes the gases and aromatic compounds collected at 500°C and identified by chromatography. It is essential to note that the given contents were normalized by removing the values corresponding to argon and residual air, as well as by not considering peaks corresponding to unknown compounds.

Table 3: Gas chromatography analyses of polymer powders pyrolysis (permanent gases and aromatics)

|  |  |  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- |
| Permanent gases  and aromatics | H2 | CH4 | CO | CO2 | C2H2 | C2H4 | C2H6 | C3H4 | C3H8 | Aromatics |
| PS Normalized volume  content (vol.%) | 2.5 | 1.9 | 6.3 | 3.1 | 0.6 | 3.1 | 0.6 | 75.2 | 3.7 | 3 |
| PE Normalized volume  content (vol.%) | 0.9 | 0 | 11.4 | 9.5 | 0.4 | 4.2 | 0.5 | 46.0 | 3.1 | 24.1 |

Low quantities of light permanent gases are generated (H2, CO, CH4...), which marks a notable difference with the natural compounds, e.g. starch and cellulose, previously studied by Pietraccini et al. (2023). On the other hand, the C3 and aromatic contents (e.g. toluene, xylene) are remarkably high. For polystyrene, it should be noted that the microGC was not calibrated to identify neither styrene, nor methylstyrene C9H12, which are two main products of PS pyrolysis (Artetxe et al., 2015). In the case of polyethylene, the low quantity of ethylene generated is due to the low test-temperature (500 °C). Experiments at higher temperatures show a significant increase in C2H4 concentration. However, Table 3 shows that heavier compounds, especially aromatics (here toluene) should also be considered. Presence of carbon monoxide and dioxide, which can be surprising for PE, is confirmed by other studies and may be due to the presence of additives or adsorbed air (Ouiminga et al., 2009). Despite the large quantities of tar and incondensable compounds, the analysis will mainly focus on lighter species, as such heavy compounds will eventually decompose into light C1-C4 gaseous hydrocarbons at higher temperature, e.g. during an explosion (Jiang et al., 2024). By changing both the oven temperature and residence time, lumped pyrolysis mechanisms can be proposed implemented and coupled to oxidation reactions of the pyrolysis gases. Such an approach has already been applied to cellulose and starch (Pietraccini et al., 2023) and will be extended to synthetic polymers.

* 1. Conclusions

Foundations have been laid for the numerical simulation of polymer powder explosions. In parallel with the development of CFD aspects, the choice of turbulence models and mesh generation, preliminary experiments were done on polystyrene and polyethylene dusts. They suggest that the development of new mechanisms representing the flash pyrolysis of polymer is needed. From a kinetic point of view, the pyrolysis stage cannot be neglected and basic devolatilization reactions (e.g. depolymerization reaction or generation of light gases only) seem inadequate. Indeed, the range of chemical species involved is significantly broader, as demonstrated by flash pyrolysis tests. Nevertheless, there are some simplification possibilities, such as neglecting the fragmentation of polymer powders during their injection in the 20L sphere.

References

Artetxe M., Lopez G., Amutio M., Barbarias I., Arregi A., Aguado R., Bilbao J., Olazar M., 2015, Styrene recovery from polystyrene by flash pyrolysis in a conical spouted bed reactor, Waste Management, 45, 126-133.

Bind V.K., Roy S., Rajagopal C., 2012, A reaction engineering approach to modeling dust explosions, Chem. Eng. J., 625-634.

Islas A., Fernández A.R., Betegón C., Martínez-Pañeda E., Pandal A., 2022, Computational assessment of biomass dust explosions in the 20L sphere, Process Saf. Environ. Prot., 165, 791-814.

Islas A., Fernández A.R., Betegón C., Martínez-Pañeda E., Pandal A., 2023, Biomass dust explosions: CFD simulations and venting experiments in a 1 m3 silo, Process Saf. Environ. Prot., 176, 1048-1062.

Jiang B., Li J.J., Su M., Lu K., Yu C.F., Yang T., Yao Q., Ding D., 2024, Study on flame properties and molecular dynamics of MAP suppression for polyethylene dust explosion, Fuel, 366, 131347.

Khan A.M., Mohalik N.K., Ray S.K., Mishra D., Pandey J.K., Mandal S., 2024, Multiphase CFD simulation of coal dust dispersion and explosion in a 20 L explosion chamber, Lecture Notes in Mech. Eng., 547 – 557.

Li H., Chen X., Deng J., Shu C.M., Kuo C.H., Yu Y., Hu X., 2020, CFD analysis and experimental study on the effect of oxygen level, particle size, and dust concentration on the flame evolution characteristics and explosion severity of cornstarch dust cloud deflagration in a spherical chamber, Powd. Tech, 372, 585-599.

Murillo C., 2016, Experimental and numerical approaches to particles dispersion in a turbulent flow: application to dust explosions (PhD Thesis). Université de Lorraine, France.

Ouiminga S.K., Rogaume T., Sougoti M., Commandre J.M., Koulidiati J., 2009, Experimental characterization of gaseous species emitted by the fast pyrolysis of biomass and polyethylene, J. Anal. Appl. Pyrolysis, 86, 2, 260-268.

Pico P., Ratkovich N., Muñoz F., Dufaud O., 2020, Analysis of the explosion behaviour of wheat starch/pyrolysis gases hybrid mixtures through experimentation and CFD-DPM simulations, Powd. Tech., 374, 330-347.

Pietraccini M., Badu P., Tait T., Glaude P.A., Dufour A., Dufaud O., 2023, Study of flash pyrolysis and combustion of biomass powders using the Godbert-Greenwald furnace: An essential step to better understand organic dust explosions, Process Saf. Environ. Prot., 169, 458-471.

Portarapillo M., Sanchirico R., Di Benedetto A., 2021, On the pyrotechnic ignitors role in dust explosion testing: Comparison between 20 L and 1 m3 explosion vessels, Process Safety Progress, 40 (4), 289 – 295.

Quek V., Sulaiman S.Z., Che Man R., Abdul Mudalip S.K., Shaarani S., Arshad Z.I., 2022, Investigation of the LDPE dust flame propagation effected by the ethylene concentration, Mater. Today: Proc, 57, 3, 1422-1426.

Ray S.K., Mohalik N.K., Khan A.M., Mishra D., Varma N.K., Pandey J.K., Singh P.K., 2020, CFD modeling to study the effect of particle size on dispersion in 20L explosion chamber: An overview, Int. J. Min. Sci. Technol., 30, 3, 321-327.

Wang D., Qian X., Wu D., Ji T., Zhang Q., Huang P., 2020, Numerical study on hydrodynamics and explosion hazards of corn starch at high-temperature environments, Powd. Tech, 360, 1067-1078.

Zhang J., Yuan Q., Meng F., Zhang H., Ding S., Chen H., Amyotte P., Li C., Yuan C., 2024, Experimental study and numerical simulation of the combustion characteristics of dust clouds in vertical pipelines underneath unilateral obstacles, J. Loss Prev. Process Ind, 87, 105212.