

Towards Autothermal Hydrogen Production by Sorption Enhanced Methanol to Shift: A Novel Concept

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Highlights

- The H₂ productivity and energy efficiency of the WGS is significantly enhanced by the addition of methanol and removal of CO₂ in situ (SEMTS)
- Commercial Cu-Zn and novel in-house synthesized Pt/CeO₂ catalysts display excellent catalytic performance for SEMTS, in the presence of hydrotalcite-based CO₂ adsorbents
- A dynamic model is developed and validated for the simulation of a cyclically operated SEMTS reactor

1. Introduction

Hydrogen (H₂) is one of the most important raw materials for the chemical and refinery industries worldwide. In addition, the use of H₂ as an ultraclean fuel in the transport and heat sectors has the potential to provide deep carbon emission reductions [1]. This has placed an imperative on improving the efficiency of steam reforming of hydrocarbons (SRH), this process being considered the most feasible and economic route to large scale H₂ production. A typical SRH plant includes a reformer followed by a water gas shift (WGS) stage and purification section. The energy efficiency of the reformer has increased significantly in recent years but there has been little progress on the improvement of the efficiency of the shift reactors. Among the few attempts to enhance the performance of the WGS section is the methanol-to-shift (MTS) process developed by Haldor Topsøe [2], which combines the exothermic WGS and the endothermic methanol reforming aiming to minimise the energy losses while boosting the H₂ productivity (up to 25%). The efficiency of the WGS can also be enhanced if it is combined with the in situ removal of CO₂ using a solid adsorbent. This shifts the equilibrium towards the products thereby increasing the production of H₂ [3].

Recently, we have reported a detailed thermodynamic analysis of the WGS and methanol steam reforming with simultaneous CO_2 adsorption (sorption enhanced methanol-to-shift, SEMTS) under typical operating conditions for SRH [4]. The results show that adding methanol to the feed enhances significantly the amount of H₂ produced and allows for autothermal operation of the shift unit. Further H₂ enhancement is achieved by separating CO_2 in situ. In this contribution, we present the first comprehensive experimental study of SEMTS. The effects of temperature, pressure, steam, methanol addition, fraction of CO_2 removed, and energy efficiency of the shift system are investigated. The performance of different commercial shift catalysts and a series of novel in-house synthesised catalysts are assessed in the presence of hydrotalcite-based adsorbents (HTs). A dynamic model is developed and validated for the simulation of a cyclically operated SEMTS reactor.

2. Methods

Commercial mid/high temperature shift catalysts (Cu/ZnO, Fe/Cr, CoMo) and a series of novel in-house synthesized catalysts (Pt/Al₂O₃, Pt/SiO₂, Pt/CeO₂/SBA15, Pt/CeO₂/ZrO₂ and Pt/CeO₂) were tested under optimal operating conditions for SEMTS [4]. In addition, hydrotalcite based adsorbents (including novel carbon and silica supported HTs) were prepared via a co-precipitation technique (see details in [5]). Transient and steady state catalytic and adsorption experiments were carried out in a stainless steel fixed bed reactor and the product evolution was measured by online mass spectrometry. The gases were fed using mass flow controllers, and steam and methanol vapors were supplied by an electrically heated vaporisation system. Breakthrough curve responses were obtained using an automated 4-way valve. After the catalysts were activated (573 K, 10% H₂/N₂), they were screened by conducting the reverse WGS and methanol decomposition under a temperature program. Stability tests of SEMTS were carried out at 573 K and 673 K for more than 24h. The enhancement of the MTS by CO₂ adsorption was evaluated by comparing the transient H₂ production in the presence and absence of adsorbent. The catalysts and CO₂ adsorbents were characterised by a range of physicochemical techniques (e.g. BET, TGA, XRD, TEM, ICP and TPR). A one

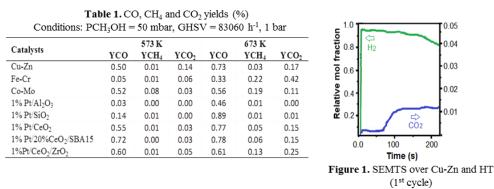


dimensional dynamic reactor model was developed to describe the performance of the SEMTS experimental results. The model was solved using gPROMS.

3. Results and discussion

The CO, CH₄ and CO₂ yields obtained at 573 K and 673 K during the TPR-methanol decomposition over the different catalysts tested are presented in Table 1. The mid-temperature Cu-Zn catalyst shows high conversions of methanol to CO and H₂ between 573 and 773 K with a negligible methane production. The amount of CO₂ produced is likely to be associated to the Boudouard reaction and α -brass alloy formation. The high temperature Fe-Cr catalyst is less active than Cu-Zn, and produces significant CO₂ and methane at high temperature. Pt/Al₂O₃ and Pt/SiO₂ are inactive at 573 K but high conversions and remarkable selectivities to CO are observed between 673 and 773 K. The negligible formation of CO₂ is related to the non-reducibility of the supports under the conditions tested. In the presence of cerium oxide the activity of Pt at low temperatures is enhanced significantly while CO₂ formation increases very modestly. Co-Mo is found to be active under methanol decomposition but relatively high amounts of methane and CO₂ are detected. MoS₂ is known to catalyze the synthesis of methanol producing methane unless it is promoted with alkali metals. Analogous TPR-RWGS studies were carried out for all the catalysts (data not shown).

From the screening tests, Cu-Zn and Pt/CeO₂ are identified as the most promising candidates to catalyze the combined methanol reforming and water gas shift (i.e. MTS). Stability tests show that the activity and selectivity of both catalysts remain constant through WGS and MTS tests alone and with simultaneous CO_2 adsorption (in the presence of a HT adsorbent). It is worth mentioning that the water co-fed during MTS mitigates the deactivation of the Cu-Zn catalyst caused by carbon deposition. The transient experimental profiles (Figure 1) can be described using a dynamic sorption-enhanced reactor model. Literature rate equations for the WGS and methanol reforming reactions, and a linear driving force model can be used to describe the reaction and adsorption kinetics respectively.



4. Conclusions

SEMTS appears as a promising technology to enhance the efficiency of the shift section while a CO_2 rich stream for sequestration is produced. The findings of this study suggest that among different commercial and in-house synthesized catalysts, Cu-Zn and novel Pt containing CeO_2 are promising candidates for SEMTS. The catalysts exhibit high activities and selectivities, and are stable under the relevant operating conditions (473 to 723 K) for MTS, in the presence and absence of hydrotalcite-based CO_2 adsorbents.

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Hydrogen, water-gas-shift reaction, methanol reforming, sorption-enhancement, CO2 adsorption

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Brief CV

Dr. Diana Iruretagoyena obtained her PhD in the Department of Chemical Engineering (2014) at Imperial College London where she currently works as Research Associate. Her research focuses on the interfaces of reaction engineering, applied catalysis, separation processes and materials science combining laboratory experiments and modelling work. Overall the research deals with the study and development of new processes which aim to be economical, environmentally friendly and energy efficient. An important part of her work involves synthesis, characterization and testing of a wide range of nanostructured materials including carbon nanotubes and graphene composites, inorganic (hydro) oxides (e.g. hydrotalcites) and supported metal catalysts. The aim is to understand and tune the chemical properties and morphology of these materials so they can be successfully applied in various areas such as adsorption of CO_2 and organosulfur compounds, hydrogen production by process intensification (e.g. sorption enhanced water gas shift reaction) and catalytic production of chemical intermediates from bio-based feedstocks.

Diana's research has resulted in relevant scientific publications and has been presented in many prestigious international conferences and seminars. She is frequently invited to present her work at international forums, form part of scientific committees, join editorial boards and be reviewer in leading engineering journals. In addition, she has received several awards including the Prize for the best poster at ISCRE 22, the Julia Higgins Centenary Prize 2014 from the Department of Chemical Engineering, Imperial College London and the Springer Theses Award 2016 from Springer.

Education

2015-present	 Research Associate Imperial College London (UK), Department of Chemical Engineering, Enabling a Low-Carbon Economy via Hydrogen and CCS (H2020, European project) Supervisor: Prof. Nilay Shah (Head of Department) Catalytic routes to intermediate sustainable process (EPSRC, UK) Supervisor: Prof. David Chadwick
2010-2014	 PhD in Chemical Engineering (Julia Higgins Centenary Prize) Imperial College London, UK, Department of Chemical Engineering. Supervisors: Prof. David Chadwick and Prof. Klaus Hellgardt Thesis: Supported Layered Double Hydroxides as CO₂ Adsorbents for Sorption- enhanced H₂ Production
2007-2009	 M.Sc in Chemical Engineering, (1st class honours) Universidad Nacional Autónoma de México (UNAM), Department of Chemical Eng. Catalytic dimerization of pentenes using fluorinated alumina
2002-2006	 B.Sc in Chemical Engineering, (Best student among 200, Gabino Barreda Medal) Universidad Nacional Autónoma de México (UNAM), Department of Chemical Eng. Thermodynamic modelling of crude oil and gas blends from Mexican reservoirs"

Awards, Scholarships, Fellowships

2016 **Springer Theses Award** (Recognizing Outstanding Ph.D. Research, *the "best of the best"*), this series publishes annually the best theses of top-ranked institutes, each thesis is selected for its scientific excellence and impact on research. (<u>http://www.springer.com/gb/book/9783319412757</u>)

2015	Associate Fellow of the Higher Education Academy (UK Professional Standards Framework)
2015	Julia Higgins Centenary Prize (Imperial College London): PhD thesis of exceptional merit in the broad areas of polymer science and materials engineering
2012	Prize for best poster at the 22 nd International Symposium on Chemical Reaction Engineering (ISCRE 22). Work presented: Supported Hydrotalcites for Sorption Enhanced Water Gas Shift Reaction
2007-2014	Scholarships awarded by CONACyT, SEP (Mexico) and ICL (UK) to study MEng. and PhD
2008	Gabino Barreda Medal in Chemical Engineering (B.Sc.).: Highest award given by UNAM to the best student of each class of every bachelor

Publications

Books

- 1. Book chapter: <u>D. Iruretagoyena</u>*, R. Montesano, Selective sulphur removal from liquid fuels using nanostructured adsorbents, In Principles and applications of nanotechnology in oil and gas industries. invited Chapter, Springer (2017), in press
- 2. Book: <u>D. Iruretagoyena</u>*, Supported Layered Double Hydroxides as CO₂ Adsorbents for Sorption-Enhanced H₂ Production, **Springer Theses (2016), Switzerland**, http://www.springer.com/gb/book/9783319412757

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Conferences

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