

Low Temperature H₂S Removal from CO with High Activity Sorbent

Pankaj Gautam^{1*}, Zhe Sun² and Tian Gu¹

¹ SABIC, Sugarland, TX 77478, United States; ² University of Houston, Houston, TX 77204, United States

*Corresponding author: pgautam@sabic.com

Highlights

- Sorbent found to effectively remove H₂S from CO at near ambient temperature (<50°C).
- A mathematical model developed and validated using literature and experimental data.
- Analytical solution derived for predicting breakthrough time.
- Parametric studies showed impact of various design parameters and operating conditions.

1. Introduction

Hydrogen sulfide H₂S is a common impurity found in chemical feedstocks that poisons many common industrial catalysts. Although extensive research has been carried out to remove H₂S from gas mixtures, particularly natural gas, no study reports H₂S removal at ambient temperatures specifically from CO stream in our knowledge. Such conditions occur while removing H₂S from the gas mixture produced out of incomplete combustion of petroleum coke. Among various reactive sorbents commonly used in natural gas desulfurization [1], we found one reactive sorbent that effectively removes H₂S from a reducing CO stream at ambient temperatures.

2. Methods

Reactive sorbents are tested in lab-scale reactors at 40°C under 8.6 barg pressure, with a feed of 95% CO, 4.9% CO₂ and ~1000 ppm H₂S. Sulfur breakthrough is monitored at the exit and experiments are stopped when either H₂S or COS breaks through.

The unreacted core model [2, 3] is used to describe H₂S capture process in reactive sorbents, with the apparent reaction rate determined by the combination of external mass transfer, intra-particle diffusion and surface reaction. An analytical solution is obtained using simplifying assumptions.

3. Results and discussion

As shown in Fig. 1, the selected reactive sorbent shows high efficiency in H₂S removal at low temperature, where the breakthrough occurs at $t \approx 30$ h and the exit H₂S level is below 30 ppm for 100 hours. Model parameters are fitted to the experimental data. Due to the high surface area and high operating pressure, the overall reaction rate is strongly influenced by internal and external mass transfer resistances even at low temperature. The model is used to design an industrial scale H₂S removal reactor. Impact of various design parameters and operating conditions on the bed life are studied, with some important ones shown in Fig. 2. In the regime of intra-particle diffusion control, an analytical formula is derived to relate the dimensionless bed life to the local Peclet number (P_m') and the dimensionless capacity (\hat{W}),

$$\hat{t}_b = \frac{t_b}{\tau} = 1.12\hat{W} \left[1 - \frac{(ab)^3(2ab - a + 2)}{2(ab + 1)^2(ab - a + 1)^2} \right]; \quad a = 1 - \frac{\omega_{H_2S}^{out}}{\omega_{H_2S}^{in}}; \quad b = \frac{P_m'}{12(1 - \epsilon)}; \quad \hat{W} = \frac{\rho_b W}{\rho_f \omega_{H_2S}^{in}}; \quad P_m' = \frac{d_p^2}{D_{eff} \tau}$$

The analytical correlation (dashed lines) shows very good agreement with detailed model results (markers).

4. Conclusions

We have discovered a reactive sorbent that effectively removes H₂S from CO stream at near ambient temperature. A mathematical model is developed and validated using experimental data, then simplified to an analytical formula to predict bed life.

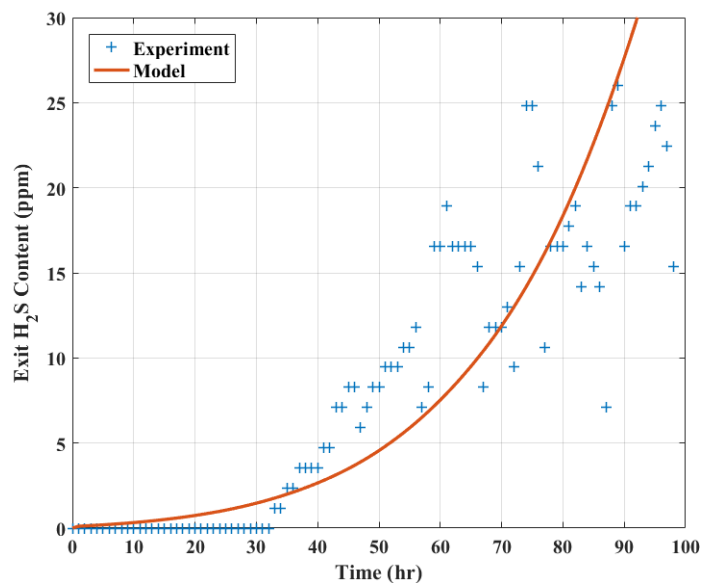


Figure 1. Breakthrough curves for the selected sorbent.

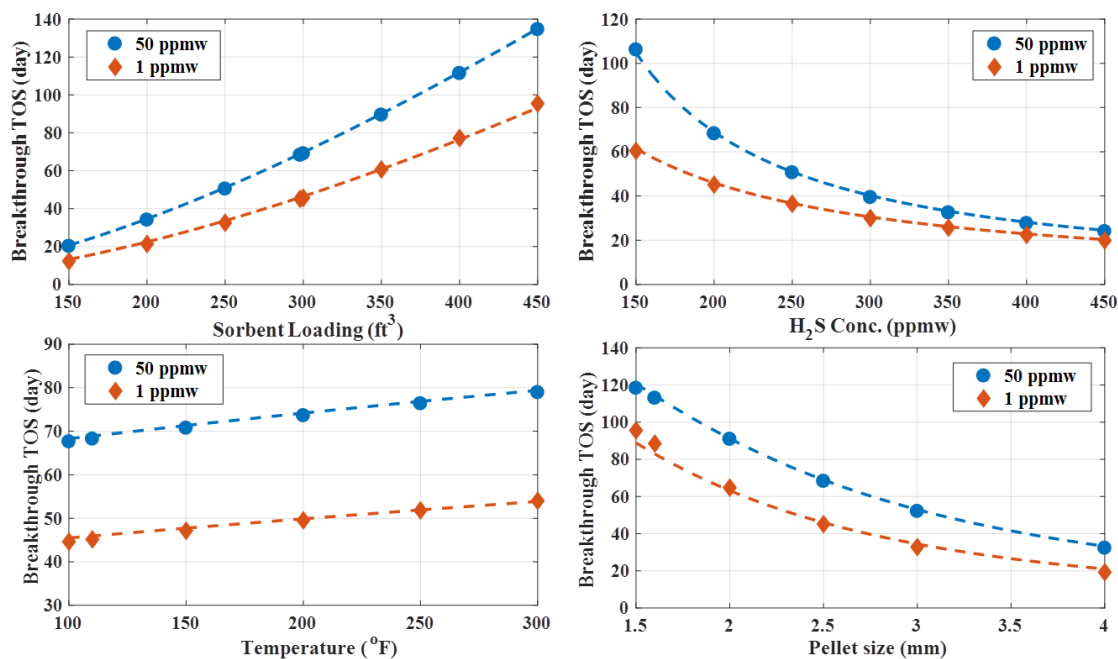


Figure 2. Impact of various parameters on breakthrough time. Numerical model results are shown in markers and the analytical correlation results are shown in dashed lines.

References

- [1] A. Samokhvalov, B.J. Tatarchuk, Phys. Chem. Chem. Phys. 13.8 (2011) 3197-3209.
- [2] I.I. Novochinskii, C. Song, X. Ma, X. Liu, L. Shore, J. Lampert, R.J. Farrauto, Energy & Fuels, 18 (2004) 576-583
- [3] I. Rosso, C. Galletti, M. Bizzi, G. Saacco, V. Specchia, Ind. Eng. Chem. Res., 42(2003)1688-1697.

Keywords

Desulfurization; H₂S removal; Reactor modeling