

## Effect of Operating Conditions on Crystal Growth in an Airlift Loop Crystallizer

Weipeng Zhang<sup>1,2\*</sup>, Tianrong Cao<sup>1,3</sup>, Jingcai Cheng<sup>1</sup>, Chao Yang<sup>1,3\*</sup>, Zai-Sha Mao<sup>1</sup>

*1 Key Laboratory of Green Process and Engineering, Institute of Process Engineering, Chinese Academy of Sciences, Beijing 100190, China*

*2 Nanjing Jiuzhang Chemical Technology Co. Ltd., Nanjing, Jiangsu 21180, China*

*3 University of Chinese Academy of Sciences, Beijing 100049, China*

*\*Corresponding author: [wzhang@ipe.ac.cn](mailto:wzhang@ipe.ac.cn); [chaoyang@ipe.ac.cn](mailto:chaoyang@ipe.ac.cn)*

### Highlights

- There is a optimum value of  $V_N$ , pH and  $D_d$  on grain growth size of  $\text{Ni}(\text{OH})_2$ .
- The gas-liquid separation zone has the best micro-mixing effect.
- With the increase of gas flow rate  $Q_G$ , the grain size  $D$  grow faster.

### 1. Introduction

Airlift loop reactors have been widely used in industry and paid more attention as crystallizers recently, because of their simple structure, efficient mixing and good mass/heat transfer characteristics [1-3]. Nickel hydroxide,  $\text{Ni}(\text{OH})_2$ , is an important crystalline material for advanced energy conversion and storage, extensively used as cathode material in rechargeable alkaline batteries [4].

In this work, the effects of operating conditions on crystal growth in an airlift crystallizer are studied using  $\text{Ni}(\text{OH})_2$  as a model.  $\text{Ni}(\text{OH})_2$  particles prepared in different conditions are measured by XRD. Then, the sizes of crystallites of  $\text{Ni}(\text{OH})_2$  ( $D$ ) are gotten by the Scherrer formula and the variations of  $D$  with the volume of ammonium hydroxide ( $V_N$ ), pH, feeding method, height of draft tube ( $H_d$ ) and gas flow ( $q_g$ ) are analyzed one by one. The main conclusions have been elaborated.

### 2. Methods

A schematic diagram of the ALR is shown in Fig. 1. The reactor is composed of an outer cylinder of diameter  $D_1=200$  mm and height of  $H_1=400$  mm, a draft tube of diameter  $D_2=120$  mm and height of  $H_2=300$  mm, and an air distributor. The clearance between the reactor bottom and the draft tube is 50 mm.

Before the start of an experimental run, distilled water is heated to the required temperature in an electric kettle and then added into the reactor, and air begins to bubble in through the distributor. After the temperature is stabilized, the  $\text{NH}_3$  and  $\text{NaOH}$  ( $0.2 \text{ mol}\cdot\text{L}^{-1}$ ) solution is added into the reactor to adjust pH value. Then,  $\text{NiSO}_4$  is added into the reactor with the feed rate of 55 mL/h and reaction begins to happen. Besides, the  $\text{NH}_3$  and  $\text{NaOH}$  ( $0.2 \text{ mol}\cdot\text{L}^{-1}$ ) solution is added continuously throughout the whole process to maintain the pH value. Samples are taken every 4 hours for tests including XRD, PSD (particle size distribution), SEM and tap density.

### 3. Results and discussion

We take the effect of addition of  $V_N$  as an example. Figure 2 shows the XRD map changes of nickel hydroxide with  $V_N$ . Under different amount of  $V_N$ , the crystal shapes of the obtained particles are all beta- $\text{Ni}(\text{OH})_2$ . With the gradual increase of  $V_N$ , the positions of each crystal surface overlap with the standard peaks, and the half width becomes narrower gradually; when the  $V_N$  increases to 500 mL, the half width becomes wider and wider. The impurity peak appears near (001) crystal surface, which is the peak corresponding to  $\text{NiSO}_4\cdot 7\text{H}_2\text{O}$  crystal (111) crystal face. Fig. 3 shows that the size of crystallite varying with  $V_N$ , which indicates that  $D$  increases firstly and then decreases with the rising of  $V_N$ . As for pH and  $H_d$ ,  $D$  varies with them according to the same trend as with  $V_N$ . When  $V_N=300$  mL, pH=11.4,  $H_d=250$  mm, the sizes of  $\text{Ni}(\text{OH})_2$  crystallites get to the maximum value.

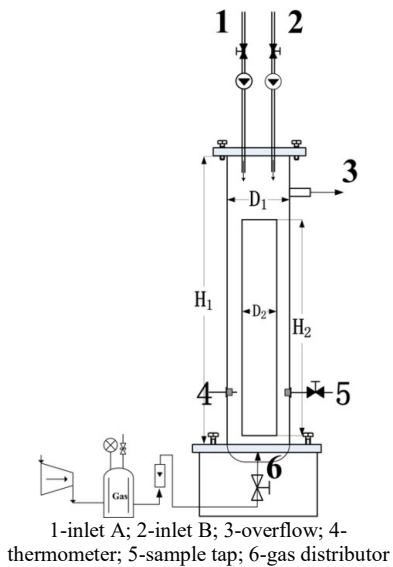


Figure 1. Schematic diagram of the ALR under investigation.

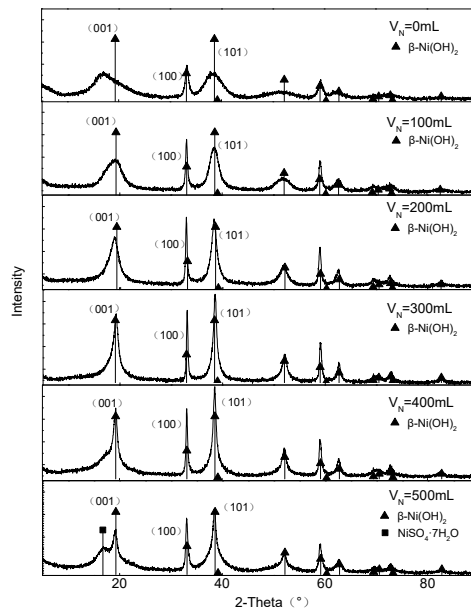


Figure 2. XRD maps of nickel hydroxide with the change of  $V_N$

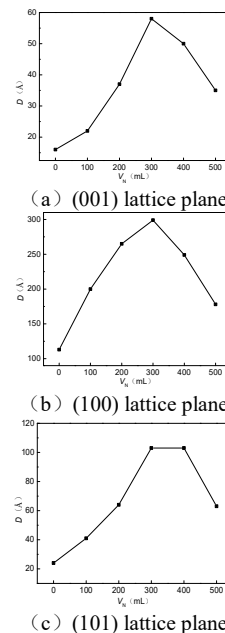


Figure 3. The size of crystallite varying with  $V_N$ .

#### 4. Conclusions

The effects of initial ammonia additions  $V_N$ , pH value, feeding method, draft tube length  $H_d$  and gas flow rate  $q_g$  on the grain growth of  $Ni(OH)_2$  in the circulation crystallizer were investigated. The grain size of  $Ni(OH)_2$  particles increases first and then decreases with the increase of  $V_N$ , pH and  $H_d$  value. The micro-mixing in gas disengagement zone is the most efficient, the crystallites grow up quicker when the feeding position is located there. Gas flow has an important effect on the growth of crystallites. The  $Ni(OH)_2$  crystallites grow up bigger with the increasing of gas flow rate  $q_g$ .

#### Acknowledgement

Financial support from the Major National Scientific Instrument Development Project (21427814), the National Key Research and Development Program of China (2016YFB0301701), the Research project of scientific research equipment of Chinese Academy of Sciences (201641) and the National Nature Science Foundation of China (91534117) are gratefully acknowledged.

#### References

- [1] Q.S. Huang, C. Yang, G.Z. Yu, Z.-S. Mao. 3-D simulations of an internal airlift loop reactor using a steady two-fluid model. *Chem. Eng. Technol.* 30 (2007) 870-879.
- [2] M. Šimčík, A. Mota, M.C. Ruzicka, A. Vicente, J. Teixeira. CFD simulation and experimental measurement of gas holdup and liquid interstitial velocity in internal loop airlift reactor. *Chem. Eng. Sci.* 66 (2011) 3268-3279.
- [3] R. Lakerveld, J.J.H. Krochten, H.J.M. Kramer. An air-lift crystallizer can suppress secondary nucleation at a higher supersaturation compared to a stirred crystallizer. *Crystal Growth Des.* 14 (2014) 3264-3275.
- [4] M. Aghazadeh, A.N. Golikand and M. Ghaemi. Synthesis, characterization, and electrochemical properties of ultrafine  $\beta-Ni(OH)_2$  nanoparticles. *Int. J. Hydrogen Energy* 36 (2011) 8674-8679.

#### Keywords

Airlift loop crystallizer; Operating conditions; Crystal growth; Nickel hydroxide