Liquid Hydrocarbon Storage Tank Fires – How Prepared is your Facility?

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A major fire is a credible scenario for any site or installation that is involved in the storage of liquid hydrocarbons (oil and fuels). Similarly, a major explosion scenario (albeit less probable than a major fire scenario with respect to hydrocarbons storage) could be considered for bulk hydrocarbon storage sites if the lessons of Buncefield explosion in 2005 are put in perspective. Obviously, major incidents like oil/fuels storage tank fires and explosions do not occur frequently; nevertheless the associated risks are ever present with attendant high impacts on people, assets and environment. Dealing effectively with these types of hazards would require a well-structured and verifiable fire hazard management (FHM) approach on one hand, and satisfactory level of emergency response preparedness on the other hand. A realistic FHM approach spanning prevention and control/mitigation measures when combined with good level of incident response preparedness (with respect to men, equipment and materials) would facilitate the reduction of associated oil storage tank fire risks to ALARP level.

Historically, the success rate of suppression and extinguishment for full surface oil tank fires is relatively low, particularly for larger tanks with diameters greater than 30 m. The only known large tank fire ever extinguished was the Orion refinery tank fire (circa 82 m diameter) in 2001. Suppressing oil tank fires is no simple task, and failures to achieve suppression timely are due to many factors most of which could have been addressed with suitable risk perception, evaluation, education and management. Poor risk perception could blindside operator’s site or corporate management to the extent that oil tank fire incident may be considered as very remote possibility or to assume that the provision of fixed and portable fire systems and a fire brigade are enough risk controls for oil tank fires. Managers of hydrocarbons bulk storage facilities need to be educated on the scale of oil tank fire hazards including but not limited to tank rupture/collapse, explosion, and boil over, and the associated challenges and competencies required to manage industrial catastrophic events of such magnitude.

This paper is therefore set to highlight the scale of threat posed to people, assets, business continuity and the environment by hydrocarbon storage tank fires, and discuss the main tank fire hazards and key factors that influence the success or failure in the prevention and suppression of oil storage tank fires

1. Introduction

Hydrocarbon storage tank fires present peculiar hazards that should require owners and managers of such facilities to exercise adequate diligence with respect to the prevention, protection and emergency preparedness suitable for managing risks associated with hydrocarbons storage fire and explosion events. Hydrocarbons storage tank fires do not occur frequently, nevertheless such incidents still happen notwithstanding the various engineering and fire protection improvements learned from previous fire incidents and furnished in different codes and standards such as NFPA (National Fire Protection Association) and API (American Petroleum Institute).

Managing fire safety in oil storage sites goes beyond the existence of safety reports, procedures and the availability of inbuilt safety features (e.g. fixed/mobile firefighting systems and tank overflow protection). Although safe designs, operating procedures and safety reports complete with risk assessment are very important, nevertheless experience has shown that oil tank fires still occur due to lapses in prevention
measures and in some cases such fires progressed to catastrophic dimensions due to inadequacies in fire
pre-plans and emergency preparedness.
Perhaps, some of the historical oil tank fires would have been prevented or their consequences mitigated if
adequate attention had been paid to maintenance and integrity assurance of facilities on one hand, and fit for
purpose emergency preparedness reviews on the other hand. Emergency preparedness reviews shall
particularly address the adequacy or otherwise of protection against primary containment aspects including
tanks, piping, overfill protection, valves (are shutoff valves fire safe?), venting systems, roof seal, corrosion
monitoring, and pumps. Other important aspects of the emergency response review are operational controls
(adequate logistics and materials – equipment, water, foam and manpower) and administrative controls
(major accident hazard identification, pre-fire plan, tank fire training and drills for emergency response crew).

2. Types of storage tanks

Above ground and atmospheric storage tank is usually described by the nature of its roof, and the physical
properties of the stored hydrocarbon liquid. There are three main types of tanks used for storing combustible
or flammable liquids, namely:
(1) Fixed Roof Tank (Cone Roof)
(2) External Floating Roof Tank (Open Top)
(3) Internal Floating Roof Tank (Covered Top)

Flammable liquids are normally stored in floating roof tanks while combustible liquids are normally stored in
fixed or cone roof tanks.

Fixed roof tanks have vertical cylindrical sides and are covered with fixed cone-shaped roofs that are welded
to the top edge of tank shells. The roof-to-shell seam is required by API standards to be a weak seam such
that in the event of an internal explosion, the roof would separate from the tank vertical shell to prevent failure
of tank bottom seam. This design requirement prevents the tank from propelling upwards and permits the tank
to retain its contents so that any resulting fire will involve the full surface of the exposed flammable liquid.

External floating roof tanks (open top) have vertical cylindrical sides and the tank contents are covered with
floating roofs that move along shells in tandem with tank liquid level. The floating roof consists of pans that
float on pontoons or double decks that float directly on the flammable liquid surface. The floating roofs have
rim seals attached to its full perimeter, covering the space between the floating roof and the tank shell, thus
preventing escape of vapours from the tank.

The internal floating roof tank (covered top) is a combination of the fixed roof and the external floating roof
tanks. The main difference between internal floating roof and external floating roof is the incorporation of a
fixed roof in the former to protect tank contents from the atmosphere. This type of tank is typically used in the
storage of highly flammable products such as gasoline or naphtha, and can be identified by the open vents in
the tank side walls just beneath the roof joint.

3. Typical incident scenarios

Different incident scenarios associated with storage tank fires present different hazards with consequences
ranging from minor to catastrophic. The following incident scenarios are typical for hydrocarbon storage sites.
(1) Explosion – often disables fixed fire fighting systems leaving no other suppression option other than
mobile foam application
(2) Boilover – a violent and catastrophic event during prolonged crude oil tank fires. See section 6.6.
(3) Rim Seal fires – rim seal fires are common to open top tanks but could also occur in covered top tanks. It
is usually less challenging to suppress provided the roof is not destroyed by explosion or made to sink by
excessive dumping of water on the roof during firefighting.
(4) Vent fires – vent fires are associated with cone roof and covered top tanks, and usually happens when
hydrocarbon vapours escaping from vents are ignited by lightning strike.
(5) Overfill ground fires (pool fires) – overfill ground fires are common to the three main types of storage tanks
and can be as a result of tank overfill due to overfill protection equipment failure or operator error or both.
Provided the dikes are not compromised and the tank overfill detected in reasonable time, the product will be
confined to the dikes and fire would be treated as pool fire. However, if the dike walls, penetration and valves
are compromised, the burning product could escape from the dike creating possible escalation of the fire
(6) Full surface fire (unobstructed) – obtainable when floating roof sinks or when fixed top is blown away.
(7) Full surface fire (obstructed) – obtainable when the roof fails and impedes 360° access to burning surface
4. Pre-incident planning

Tank fires present formidable challenge and could escalate to complex events with catastrophic consequences if approached without effective strategy. Having an incident plan in itself does not guarantee success in tank fire fighting, unless such a plan is tested regularly and also sufficient in terms of preventive and mitigation measures as reasonably practicable. Pre-incident planning should focus on aspects such as facility layout, access to and within facility, tanks (number of, diameter, height), stored product/fuel type and inventory, environmental conditions (weather – ambient temperature, rain; flooding, wind), terrain - equipment staging and water runoff, fire scenarios including worst case scenario, firefighting equipment (fixed, mobile systems), facility location – remoteness or proximity to mutual/municipal assistance, facility fire brigade, availability of foam concentrate and other foam making and discharge materials, water supply and logistics (which is a critical success factor for oil tank fire suppression).

Site specific pre-incident desktop planning essentials include but not limited to the following:

1. Consideration of the results of emergency preparedness review, hazard identification and risk assessment based on foreseen incident scenarios – tank fire, bund fire, tank collapse etc.
2. Review of existing calculations for water/foam requirements, review of installed systems (fixed/mobile), and compare resultant requirements with available resources (materials, systems, manpower)
3. Determine the sort of firefighting policy that fits your site? – attack fire with fixed equipment or mobile equipment, pump tank inventory out, let tank burn, protect adjacent tanks etc.

5. Limitations of applicable standards

The design and installation of most fixed or semi fixed foam fire protection on storage tanks are based on NFPA 11. Provided a fixed fire installation is not damaged, it should on proper application suppress rim seal fires. However, when explosion precedes fire in storage tanks incidents, the fixed systems are most likely to be damaged thus making it impossible to suppress associated fires unless an alternative fire fighting system (mobile system) is employed.

For brevity the limitations of NFPA 11 standard are as follows:

- Monitor nozzles shall not be considered as the primary means of protection for fixed roof tanks over 18 m (60 ft) diameter (design criteria for foam monitors and hand lines)
- Fixed fire protection is likely to work for small tanks particularly for seal fire conditions
- Fixed fire protection design is solely for seal fires; NOT for full surface fires
- For full surface fires, monitors are only option for suppression
- In most cases storage tanks firefighting sized on prevailing NFPA guide involved in surface fires have been allowed to burn out

Therefore when storage tank protection is limited to fixed systems, there would be no chance to confront the fire once the system has been disabled by explosion. In this circumstance, dependence on fire truck monitors may not be effective particularly for full surface fires considering the sustained and higher rates of foam application required to produce reasonable foam bite and fire knockdown.

In the absence of mobile equipment (high volume nozzles and foam lines), storage tank fires may rage beyond the capability of the emergency response team forcing them to surrender to the fire allowing tank burnout with grave consequences of boilover for products with boilover tendencies (e.g. crude oil, hydrocarbon mixtures of different boiling points).

6. Specific storage tank fire hazards

6.1 Compromised bunds

The main focus in oil storage tank hazard management is the prevention of fire and control of fire escalation. Therefore it is fundamental that tank inventory must be kept in containment at all times and should not be let out. Failure to keep inventory within primary or secondary containments during emergencies could lead to exposure of people at site, third party people in the vicinity of the installation and the facilities to the risks of explosion and fire from spreading oil that could not be constrained by secondary containment due to integrity lapses or operational errors. Besides the basic provision of dikes that meet the requirements of tank inventory holding, attention should be paid to bund integrity (ensuring that bunds and rains are properly examined and maintained; and that dike penetrations are not compromised) and operational issues like letting the bund drain valve in open position.

6.2 Thermal fluxes and radiation

Thermal fluxes and radiation associated with storage tank fires pose significant hazards to people and facilities. People (emergency response personnel and operators) and adjacent facilities might be affected by radiation and incident thermal fluxes during tank fire incidents depending on the amount of heat released by the burning product (surface area of the fire and the product involved), distance of the fire to the receptor
(person or facility) and wind speed. Thermal radiation consequence on people could range from first degree burn injury to fatality, while consequences on facilities could involve the weakening of materials stress bearing capacity leading to structural failure and possible loss of containment of hazardous materials. Radiation level of 5 kW/m² and above is capable of causing second degree burns to people within 60 seconds of exposure (FEMA Publication, 1988) and impairs escape ability, while radiation level of 10 kW/m² and above would be potentially fatal with 60 seconds. For information on thermal radiation level of concern and associated thermal doses refer to Table 1.

**Table 1: Thermal radiation Level of Concern (bare skin basis)**

<table>
<thead>
<tr>
<th>Thermal Flux</th>
<th>Concern</th>
<th>Thermal Dose over time</th>
</tr>
</thead>
<tbody>
<tr>
<td>2 kW/m²</td>
<td>Pain in 60 seconds</td>
<td>151 in 1 minute, 1057 in 7 minutes</td>
</tr>
<tr>
<td>5 kW/m²</td>
<td>2nd degree burn in 60 seconds</td>
<td>513 in 1 minute, 1026 in 2 minutes</td>
</tr>
<tr>
<td>10 kW/m²</td>
<td>Potentially lethal in 60 seconds</td>
<td>1293 in 1 minute</td>
</tr>
</tbody>
</table>

Appropriate and sufficient control measures may include the provision of water curtains and fixed cooling water for incident heat susceptible installations (e.g. vessels/pipes and their supports). Such control measures shall be foreseen in site specific emergency response procedure, and should go beyond the control of hazards of structural collapse and loss of containment, to managing the incident heat hazard posed to people by establishing safe response threshold values for likely heat radiation levels focusing on access for fire-fighters, escape path (emergency exit) and activation of protective cooling for people. The fatality probability relating to thermal dose levels are furnished in Table 2 to underscore the need for adequate assessment and management of people’s exposure to thermal flux levels with respect to acceptable separation distances.

**Table 2: Best conservative estimates for thermal dose fatality probability**

<table>
<thead>
<tr>
<th>Fatality probability</th>
<th>Thermal Dose Unit</th>
</tr>
</thead>
<tbody>
<tr>
<td>1-5 % fatality</td>
<td>1000</td>
</tr>
<tr>
<td>50 % fatality (LD50)</td>
<td>2000. Subject to following conditions.</td>
</tr>
<tr>
<td>Clothing ignited, increasing probability for 100 % fatality.</td>
<td></td>
</tr>
<tr>
<td>Clothing not ignited, but victim receives 2nd and 3rd degree burns</td>
<td></td>
</tr>
<tr>
<td>Escape impendiment, and reduced escape dexterity</td>
<td></td>
</tr>
<tr>
<td>100 % fatality</td>
<td>3500</td>
</tr>
</tbody>
</table>

**6.3 Heat stress**

Heat stress is common hazard in fire fighting or other hot and humid environments where the body’s natural cooling efficiency could be impeded, thus triggering heat illness. Besides the heat from fire or environment, the body also generates heat during physical work, exertion or exercise. The effect of heat stress on people particularly emergency responders can be worsened by the properties of the protective clothing and continuous physical exertion. Recognizing heat stress symptoms and taking appropriate action to stop progression to heat stroke (which is medical emergency) are essential in minimizing the health effects of heat stress and heat stroke. Excerpts from (OHSCO, 2009) on heat stress symptoms are furnished in Table 3. As rule of the thumb, frequent rehydration and rest rotation are pivotal to forestalling heat illness at work.

**Table 3: Heat stress symptoms**

<table>
<thead>
<tr>
<th>Symptoms</th>
<th>Heat Exhaustion</th>
<th>Heat Stroke</th>
</tr>
</thead>
<tbody>
<tr>
<td>Medical Emergency</td>
<td>No</td>
<td>Yes</td>
</tr>
<tr>
<td>Disorientation/Confusion/Coma</td>
<td>No</td>
<td>Yes</td>
</tr>
<tr>
<td>Body temperature ≥38 °C</td>
<td>Yes</td>
<td>Yes</td>
</tr>
<tr>
<td>Dizziness/Headache/Nausea</td>
<td>Yes</td>
<td>Yes</td>
</tr>
<tr>
<td>Sweating/Skin condition (heavy)</td>
<td>Yes (heavy)/moist</td>
<td>No/ dry, hot</td>
</tr>
<tr>
<td>Rapid Pulse Rate</td>
<td>Yes</td>
<td>Yes</td>
</tr>
</tbody>
</table>

**6.4 Blast overpressure**

Blast overpressure is shock wave from an explosion due to the energy released by the explosion. It is instantaneous and travels at the speed of sound. It radiates outwards from the centre of explosion and generates hazardous missiles that may increase the scale of injuries. Excerpts from (NOAA, no date) on over pressure levels of concern are furnished in Table 5.
6.5 Toxic substances
Toxic substances are produced during fire incidents and constitute formidable hazards to firemen, emergency response resources and operating personnel. The toxicity of smoke and fumes will depend on the type of fuel and materials involved in the fire and to some extent the amount of oxygen available for combustion. Specifically for crude oil fires, the associated smoke contains a mixture of gaseous and particulate compounds including carbon dioxide, carbon monoxide, nitrogen oxides, sulphur dioxide, volatile organic compounds, polycyclic aromatic hydrocarbons, hydrogen sulphide, aerosols and soot. Health impact could range from respiratory irritation, loss of physical performance, confusion, inability to escape and chronic life threatening poisoning to immediately dangerous to life.

6.6 Boilover
Boilover is a phenomenon associated with storage tank fires where the burning product (crude oil or a blend of hydrocarbon liquids) is explosively released from the tank when the burning oil makes contact with water at the bottom of the tank. A boilover represents the worst case scenario in the event of crude oil tank on fire. Mid-range gravity crude oils or blended fuels oils with a wide range of hydrocarbons have the potential for boilover during fires that last for extended periods. When faced with potential boilover, the incident commander must consider the evacuation of people from the tank vicinity when heat wave approaches the water interface at tank bottom. Since tank wall temperature or noise are not definitive guides (LASTFIRE update, 2009) in tracking the heat wave, infrared thermal imaging camera may be employed to locate the position of the heat wave; if available. Alternatively, with respect to pre-fire tank conditions; precautionary estimates of the hot zone position could be made using a generous hot zone advance rate of 1.5 m/h. The following are typical of crude oil boilover:

1. A boilover covers approximately 10D (D is tank diameter) or more (LASTFIRE update, 2009)
2. The heat wave advances from the top towards the bottom of the tank at approximately 0.6 –1.0 m/h

Table 5: Blast overpressure Level of Concern

<table>
<thead>
<tr>
<th>Overpressure (psig)</th>
<th>Concern</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.0 – 2.5</td>
<td>Partial damage of houses; shattered glass, metal and wood panels buckle and blown off respectively; brickwork and non-reinforced concrete shattered. Damage to roof of storage tank (including fixed firefighting system), rupture of storage tank</td>
</tr>
<tr>
<td>2.5 – 12.0</td>
<td>Up to 90 % eardrum rupture among exposed population</td>
</tr>
<tr>
<td>5.0 – 7.0</td>
<td>Near complete destruction of houses</td>
</tr>
<tr>
<td>14.0 – 29.0</td>
<td>Up to 99 % fatality among exposed population Collapse of supporting structure of storage tanks Demolition/severe damage of reinforced/heavily built concrete buildings</td>
</tr>
</tbody>
</table>

Figure 1: Boilover mechanism
7. Learned lessons

In the aftermath of the Buncefield fire incident, many tank operators and owners of liquid hydrocarbon storage sites are yet to learn the lessons of that incident. Devastating tank fires have continued to occur, catching operators off-guard and exposing lack of forethought, expertise and preparedness of victim organizations. Some notable post-Buncefield tank fire incident include but not limited to Amuay (Venezuela) refinery explosion and tank fires – 2012, Jaipur (India) tank farm fire disaster – 2009, Porto Rico tank farm disaster – 2009 and most recently Kiev (Ukraine) oil depot fire disaster – June 2015.

For brevity, lessons that ought to be learned from numerous hydrocarbon storage tank fires include but not limited to the following:

- **NFPA limitations** – recognizing NFPA limitations with respect to fire fighting sizing for tanks (i.e. fixed system which is often rendered dysfunctional by fire/explosion, not sized for surface fires) and making appropriate provisions for combating full surface fires which can only be suppressed with
- **Logistics** – represents the greatest challenge. Portable high-volume water and foam long range monitors, high-volume fire water relay pumps and hoses, adequate stock or availability of foam concentrate (best packed in totes) based on fire pre-plan assessment and continuous water supply are imperative for meaningful fire suppression effort.
- **Foam quality** – foam is the sole extinguishing agent whose quality must consistent and proven to be effective. It is prudent to carryout foam performance tests to check foam quality and verify manufacturers claims as poor foam quality is easily broken down or disrupted by light winds leading to prolonged extinguishing times and can present dangerous exposure for firemen.
- **Emergency preparedness review** – comprehensive and periodic reviews of preparedness in vital aspects such as containment (primary and secondary), equipment, logistics, fire pre-plans and crew training for oil tank fires

8. Conclusions

Tank fire incidents may not be frequent but they still happen even in the post Buncefield era, some with devastating consequences. Recent tank fires continue to expose organizational lapses in preventive measures particularly inadequacy in maintenance and integrity assurance of primary/secondary containment and other engineered safety systems. Further organizational lapses relating to inadequate operational controls, inadequate logistics, absence of suitable and tested pre-fire plan and poor tactical approach occasioned by inadequate training and experience of the crew all combine to permit tank fire escalation with serious consequences for personal safety, assets, environment and business continuity.

Oil tank fire emergency is completely different from structural fire emergency, therefore effective control of tank fires would require the intervention of competent crew with the requisite knowledge and experience in combating tank fire. In extinguishing the Orion refinery tank fire, Williams Fire demonstrated the importance of knowledge and experience in tank fire emergency (utilizing high volume pump and foam monitors with modified NFPA foam requirements). Therefore, for any operator or organization to successfully respond to tank fire emergencies, adequate attention must be paid to fire pre-planning, crew training, emergency preparedness reviews and regular testing of response plans.

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