

VOL. 56, 2017



DOI: 10.3303/CET1756210

Guest Editors: Jiří Jaromír Klemeš, Peng Yen Liew, Wai Shin Ho, Jeng Shiun Lim Copyright © 2017, AIDIC Servizi S.r.l., **ISBN** 978-88-95608-47-1; **ISSN** 2283-9216

# Effect of Washing Pre-treatment of Empty Fruit Bunch Hydrogel Biochar Composite Properties as Potential Adsorbent

Nor Hidayah Meri\*,<sup>a</sup>, Azil Bahari Alias<sup>a</sup>, Norhayati Talib<sup>a</sup>, Zulkifli Abdul Rashid<sup>a</sup> Wan Azlina Wan Abdul Karim Ghani<sup>b</sup>

<sup>a</sup>Faculty of Chemical Engineering, Universiti Teknologi MARA, 40450 Shah Alam, Selangor, Malaysia <sup>b</sup>Department of Chemical & Environmental Engineering, Faculty of Engineering, Universiti Putra Malaysia, 43400 Serdang, Selangor, Malaysia norhidayahmeri@yahoo.com

Hydrogel biochar composite (HBC) showed a great potential as effective organic contaminant removal in various wastewater and gas treatment. The effectiveness is depending upon quality of biochar used during the preparation of the HBC. In this work, pre-treatment of the biochar samples (EFB in this case) through washing was investigated. The raw EFB biochar was prepared using microwave assisted pyrolysis under 1,000 W for 30 min under N<sub>2</sub> flow with 150 mL/min. The prepared biochar is chemically treated using either acid solution (HCI) or oxidising agent (H<sub>2</sub>O<sub>2</sub>) to enlarge the pores and remove impurities. The biochar is then polymerised by using acrylamide (AAm) as monomer, N,N'-methylenebisacrylamide (MBA) as crosslinker and ammonium persulfate (APS) as initiator to form the treated hydrogel biochar composite (EFB-HBC). The H<sub>2</sub>O<sub>2</sub> treated biochar [EFB-HBC (P100)] shows better porosity compared to HCI treated biochar [EFB-HBC (H100)] where EFB-HBC (P100) has higher surface area (1.5997 m<sup>2</sup>/g) compared to EFB-HBC (H100) (1.2562 m<sup>2</sup>/g). The HBC is porous and carbonaceous material with 21 % and 31 % of carbon content in EFB-HBC (P100) and EFB-HBC (H100) which have potential as an adsorbent in wastewater and gas treatment.

## 1. Introduction

Biochar is highly porous material and has been studied as activated carbon for various adsorption of inorganic pollutants, heavy metals, dyes and hazardous gas (Kołodyńska et al., 2012). Hunt (2010) stated that biochar contain stable carbon and have good potential in adsorption which can attract the molecule, in the same time, remove the hazardous molecule but limited to low adsorption rate due to the low active site and post separation in handling saturated biochar adsorbents. HBC is a unique material in terms of physical and chemical properties because it is hydrophilic, swell able and modifiable composite (Okay, 2010). In recent years, HBC was become research interest in the development and application of this material in wastewater and gas treatment as potential novel adsorbent. As presented by Sanyang et al. (2014), the experiment was successful with 99 % and 35.75 mg/g sorption capacity of zinc removal in wastewater by modified RH-HBC (hydrogel biochar composite form rice husk). As stated in a review by Tan et al. (2015), the concentrations of extractable toxic elements such as polycyclic aromatic hydrocarbon (PAH) is contained within the biochar which affected by the preparation of biochar itself especially in pyrolysis process. The aim of this study is to enhance the performance of biochar as adsorbent in washing pre-treatment with 0.1 M HCl and 0.1 M H<sub>2</sub>O<sub>2</sub> in order to remove the impurities, toxic element and enlarge the porosity. The dilute acid such as 0.1 M HCl is suitable to use because it could prevent the damage of lignocellulose and can protect the structure of biochar (Sadaka, 2008). H<sub>2</sub>O<sub>2</sub> (Peroxide) is chosen because it is an oxidising agent which have potential to bleach and in the same time will remove the impurities (Diaz et al., 2013). This study will compare and investigate the effect of washing pre-treatment biochar by using HCI and H<sub>2</sub>O<sub>2</sub> in the formation of hydrogel Biochar Composite (HBC). Biochar that washed by H<sub>2</sub>O<sub>2</sub> should get a good result in term of porosity and pore structure and

1255

1256

minimise the amount of toxic element because  $H_2O_2$  will oxidising some lignins, cyanides, sulphides and phenols (Rust, 1959).

## 2. Material and Method

### 2.1 Raw Material & Chemical

Empty Fruit Bunch (EFB) used in this study was obtained from one of the palm oil industry located in Banting, Selangor. The washing agent for this study are 0.1 M of dilute Hydrochloric acid (HCl) and 0.1 M Hydrogen Peroxide (H<sub>2</sub>O<sub>2</sub>) for biochar pre-treatment and distilled water is used as diluting agent. Other chemicals for HBC synthesise, such as Acrylamide (AAm) as monomer, N,N'-methylenebisacrylamide (MBA) as cross-linker and ammonium persulfate (APS) as initiator, are supplied from R&M chemical.

### 2.2 Biochar

Biochar were prepared using microwave assisted pyrolysis technique. 200 g of raw Empty Fruit Bunch (EFB) were placed in quartz reactor in the microwave pyrolyser at 1,000 W of microwave power level 30 min under nitrogen flow at 150 mL/min. The method is modified from Januri et al. (2014).

### 2.3 Acid Washing Pre-treatment

The acid washing experiments were carried out using Hydrochloric Acid (HCl) and Hydrogen Peroxide  $H_2O_2$  (Yakout et al., 2015). 2 L of diluted 0.1 M HCl and 2 L of 0.1 M  $H_2O_2$  solutions were prepared in 2 L volumetric flask separately for stock chemical solution. 10 g of EFB biochar were pre-treated with 200 mL of prepared acid solutions in a closed beaker for 6 hrs. The biochar were washed with distilled water until a neutral pH is obtained and oven dried at 80 °C overnights. The HCl and  $H_2O_2$  treated biochar are named as biochar H100 and biochar P100.

### 2.4 Hydrogel Biochar Production

EFB-HBC were synthesised by dissolving 1.0 g of AAm in 1.0 mL of distilled water. Then, 0.6 g of Empty Fruit Bunch (EFB) biochar and 0.001 g of MBA were added to the AAm solution. After thorough mixing, 0.2 mL of 0.1 g aqueous solution of APS was added to initiate the polymerisation. The hydrogel biochar precursor solution was immediately placed into a plastic mould and placed in an oven at 40 °C for 30 min. The hydrogel biochar composites were removed from the oven and left for 24 h at room temperature to ensure the complete polymerisation and crosslinking. EFB-HBC was taken out from the plastic mould, cut into desired sizes and washed several times with the distilled water to remove all unreacted monomers and low molecular weight polymeric matters from the hydrogel. The washed EFB-HBC was air dried before drying in a vacuum oven at 40 °C for 24 h. The HCI and H<sub>2</sub>O<sub>2</sub> treated hydrogel biochar are named as EFB-HBC H100 and EFB-HBC P100. This hydrogel formation method is adapted from Karakoyun et al. (2011).

### 2.5 Characterisation

The characterisation of the morphology trend of pores on the surface of samples was done on raw EFB, EFB biochar, EFB biochar pre-treated with HCl (biochar H100), EFB biochar pre-treated with H<sub>2</sub>O<sub>2</sub> (biochar P100), EFB-HBC H100 and EFB-HBC P100 by using the Field Emission Scanning Electronic Microscopic (FESEM) (model SUPRA 40VP). FESEM was operated in accelerating voltage and the working distances used were 5 kV and 5 mm. Before proceed the FESEM analysis, all the samples were coated with gold in order to remove any residual ions on the samples. The image was captured under magnification of 500X in 10  $\mu$ m size. The characterisation on surface area (m<sup>2</sup>/g), pore volume (m<sup>3</sup>/g) and average pore size (Å) was analysed by Brunauer-Emmett-Teller (BET) method (model Micromeritic 3 flex). The BET method is operated with Nitrogen (N<sub>2</sub>) adsorption and desorption at room temperature. The maximum temperature of samples and element content such as, moisture content, volatile matter content, carbon content and ash content were determined and analysed by Thermogravimetry Analysis (TGA) under 10 °C/min of proximate gas with initial sample mass of 20 mg.

### 3. Results and Discussions

Figure 1 shows SEM image for all samples. The enlargement of pore was observed after the pyrolysis of raw EFB to biochar (Figure 1(a) and 1(b)). According to Sadaka (2008), the enlargement is caused by the breakdown of cellulose, hemicellulose and lignin during the pyrolysis process to form the volatile products with low molecular weight. Figure 1(c) shows the pore structure after HCI washing pre-treatment (biochar H100), no much different were observed between biochar H100 and biochar. The pores formed after  $H_2O_2$  washing pre-treatment (biochar P100) (Figure 1(d)) were bigger compared to biochar and biochar H100.  $H_2O_2$  is an

oxidising agent and alkaline peroxide which can remove partial lignin and make the hemicellulose wall became thinner (Diaz et al. 2013). Figure 1(e) and 1(f) show the SEM image of EFB-HBC H100 and EFB-HBC P100. EFB-HBC H100 have thicker lignocellulose wall compared to EFB-HBC P100 and Gunawan et al. (2009) have stated that, these lignocellulosic fibre has characteristics such as good tensile strength and strong cellulose backbone (Gunawan et al., 2009). With the synthesis of HBC, the lignocellulose wall becomes stronger and protected by the presence of cross-linker. The SEM image results shows that, EFB-HBC P100 have a potential as an adsorbent since the ability of adsorption will depends on the surface area and pore structure (Rafatullah et al., 2010).



(a) Raw Empty Fruit Bunch (EFB)



(b) Empty Fruit Bunch Biochar

(e) EFB-HBC H100 (HCI)



(f) EFB-HBC P100 (Peroxide)

Pa 2 + 26.07 µm Po 2 = 100.6 * Pa R	XXXX	2000
	KOK	y not
	QD7	1784
Pa 2 = 15.00 µm		Pe 1 = 31 30 um Pis 1 = 328 51
Quer		BOH

(d) Pre-treated Biochar with Peroxide ( $H_2O_2$ ) (Biochar P100)

Figure 1: SEM Image

Material	BET surface area, m <sup>2</sup> /g	Total pore volume, cm <sup>3</sup> /g	Average Pore Size, nm
Raw EFB	1.6061	0.001729	6.6628
Biochar	1.9431	0.005851	10.4459
Biochar H100	13.6074	0.009366	3.3589
Biochar P100	111.6225	0.045540	1.7544
EFB-HBC H100	1.2562	0.000951	3.0272
EFB-HBC P100	1.5997	0.000965	3.8381

Table 1 shows the results of BET surface area, total pore volume and average pore size for all samples. EFB-HBC P100 shows a higher BET surface area ( $1.5997 \text{ m}^2/\text{g}$ ) and total pore volume ( $0.000965 \text{ cm}^3/\text{g}$ ) than EFB-HBC H100 ( $1.2562 \text{ m}^2/\text{g}$  and  $0.000951 \text{ cm}^3/\text{g}$ ). The EFB-HBC P100 has an average pore size of 3.83805 nmwhich is higher compared to EFB-HB H100 average pore size of 3.0272 nm. The two HBCs are considered as a mesopore since the average pore sizes observed are in range between 2 to 50 nm. Figure 2 shows the type II BET isotherm for HBCs. This type of isotherm represent that, it is a uniform macropores and have strong interaction with surface (Al Othman, 2012). This can be concluded that, the BET surface area are low compared to biochar and treated biochar because of the presence of macropores on the surface structure with the size greater than 50 nm.



Figure 2: BET Isotherm for HBCs

The thermogravimetric (TG) and derivative of thermogravimetric (DTG) curves for EFB-HBC H100 and EFB-HBC P100 are shown in Figure 3 and 4. TGA results show that the peak temperatures of EFB-HBCs samples are almost the same and having the same thermal behaviour but different weight loss (%). The TG curve showed that, the thermal decomposition of EFB-HBCs is almost completed when the temperature is over 1,000 °C. This means that the HBCs can be exposed to high temperature. The first peak (25 °C < T < 135 °C) in DTG curve represent that, the mass loss is mainly due to the moisture evaporation (Rafatullah et al., 2010). DTG profile of EFB-HB H100 and EFB-HB P100 exhibited two peak temperatures around Tp,1 = 300 °C and Tp,2 = 400 °C. Around the temperature of 200 °C to 400 °C, volatile matter such as cellulose, hemicelluloses and some of polymer from hydrogel polymerisation are decomposed (Idris et al., 2010). The samples are then combusted in Oxygen at 750 °C to identify the carbon content in HBCs. Final peak at 950 °C is represented as the thermal degradation of carbon. At last, the residue left represented the ash content and some other inorganic materials in HBCs.



Figure 3: Thermogravimetric (TG) curve for EFB-HBC H100 and EFB-HBC P100



Figure 4: Derivative Thermogravimetric (DTG) curve for EFB-HBC H100 and EFB-HBC P100

Material	Moisture Content	Volatile Content	Carbon Content	Ash Content
	(%)	(%)	(%)	(%)
Raw EFB	7.82	26.82	6.44	36.08
Biochar	7.28	11.61	41.81	39.26
Biochar H100	8.81	10.99	65.05	15.14
Biochar P100	7.52	8.08	47.76	36.93
EFB-HBC H100	5.19	25.85	30.97	37.88
EFB-HBC P100	3.39	24.53	21.00	50.00

Table 2: Proximate Analysis Result for HBCs.

The proximate analysis results are provided in Table 2. It can be observed that, the decreasing moisture content are observed when treated biochar (Biochar H100: 8.81 % and Biochar P100: 7.52 %) became Hydrogel Biochar Composite (HBC) (EFB-HBC H100: 5.19 % and EFB-HBC P100: 3.39 %). After polymerisation process, the increased of volatile matter were when treated biochar (Biochar H100: 10.99 % and Biochar P100: 8.08 %) became HBC (EFB-HBC H100: 25.85 % and EFB-HBC P100: 24.53 %). EFB-HBC H100 has higher carbon content whish is 30.97 % compared to EFB-HBC P100 (21 %). The reason is that the  $H_2O_2$  treated biochar had oxidised some amount of carbon in the EFB biochar. EFB-HBC P100 has a higher ash content which is 50 % compared to EFB-HBC H100 which is only 37.88 %.

### 4. Conclusion

The combination of hydrogel and biochar give a new modified adsorbent in order to improve the adsorption capacity. Washing pre-treatment of EFB biochar before synthesised the HBCs give some improvement on pore structure and BET surface area especially the  $H_2O_2$  treated EFB biochar (Biochar P100). EFB-HBC P100 has higher BET surface area (1.5997 m<sup>2</sup>/g) compared to EFB-HBC H100 (1.2562 m<sup>2</sup>/g). SEM image showed that the pore structure of biochar P100 and EFB-HBC P100 was increased with thin lignocellulose wall. The pore structure become stronger and protected by presence of cross-linker after synthesised to EFB-HBC P100. Although HBCs were categorised under lower BET surface area, HBCs can be a potential adsorbent with the presence of uniform macropores and strong interaction with surface. The TGA showed that, HBCs is a carbonaceous material which can exposed to temperate greater than 1,000 °C.

#### Acknowledgment

This research was supported by a grant 600-RMI/FRGS 5/3 (96/2014). We would like to thank to Ministry of Higher Education (MOHE), Universiti Teknologi Mara (UiTM) and Faculty of Chemical Engineering for the grant sponsorship, facilities and motivation.

#### References

- Al Othman Z.A., 2012, A review: Fundamental aspects of silicate mesoporous materials, Materials 5 (12), 2874-2902.
- Diaz A., Le Toullec J., Blandino A., de Ory I., Caro I., 2013, Pretreatment of rice hulls with alkaline peroxide to enhance enzyme hydrolysis for ethanol production, Chemical Engineering Transactions 32, 949–954.
- Hunt J., DuPonte M., Sato D., Kawabata A., 2010, The Basics of Biochar: A Natural Soil Amendment, Soil and Crop Management 30 (4), 1-6.
- Idris S.S., Abd Rahman N., Ismail K., Alias A.B., Abd Rashid Z., Aris M.J., 2010, Investigation on thermochemical behaviour of low rank Malaysian coal, oil palm biomass and their blends during pyrolysis via thermogravimetric analysis (TGA), Bioresource Technology 101 (12), 4584-4592.
- Januri Z., Abdul Rahman N., Idris S.S., Matal S.i, Fairuz Abdul Manaf S., 2014, Microwave Assisted Pyrolysis (MAP) of Automotive Paint Sludge (APS), Jurnal Teknologi 5 (8), 103-109.
- Karakoyun N., Kubilay S., Aktas N., Turhan O., Kasimoglu M., Yilmaz S., Sahiner N., 2011, Hydrogel –Biochar composites for effective organic contaminant removal from aqueous media, DES 280 (1-3), 319-325.
- Kołodyńska, D., Wnetrzak R., Leahy J.J., Hayes M.H.B., Kwaspinski W., Hubicki Z., 2012, Kinetic and adsorptive characterization of biochar in metal ions removal, Chemical Engineering Journal 197, 295-305.
  Okay O., 2010, General Properties of Hydrogels, Hydrogel Sensors and Actuators 6, 1-14.
- Rafatullah M., Sulaiman O., Hashim R., Ahmad A., 2010, Adsorption of methylene blue on low-cost adsorbents: A review, Journal of Hazardous Materials 177 (1–3), 70-80.
- Rust F.F., 1959, The manufacture of hydrogen peroxide, Filtration, 1-6.
- Sadaka S., Boateng A.A., 2008, Pyrolysis and Bio Oil, University of Arkansas <www.uaex.edu/publications/ pdf/fsa-1052.pdf> assessed 18.11.2016.
- Sanyang L., Wan Ab Karim Ghani W.A., Idris A., Mansor A., 2014, Zinc Removal from Wastewater Using Hydrogel Modified Biochar, Applied Mechanics and Materials, 625, 842-846.
- Tan X., Liu Y., Seng G., Wang X., Hua X., Gua Y., Yang Z., 2015, Application of biochar for the removal of pollutants from aqueous solutions, Chemosphere 125, 70-85.
- Yakout S.M., Daifullah A.E.H.M., El-Reefy S.A., 2015, Pore Structure Characterization of Chemically Modified Biochar Derived From Rice Straw, Environmental engineering and management journal 14 (2), 473-480.

#### 1260